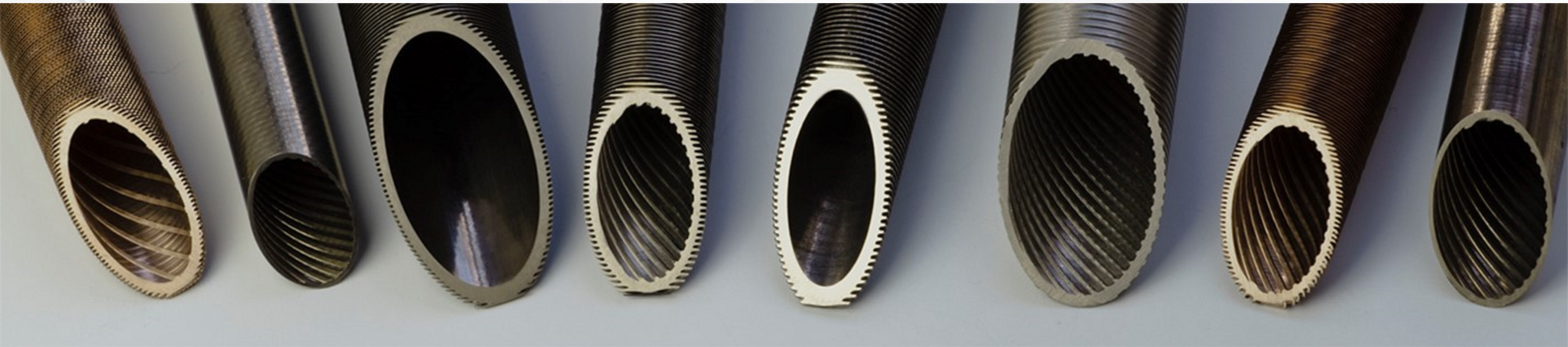


IMPROVING HEAT EXCHANGER EFFICIENCY WITH INTERNALLY ENHANCED HEAT EXCHANGER TUBING



Sponsored by:



Types of Internal Tube Enhancements



Turbulators / Inserts



Twisted

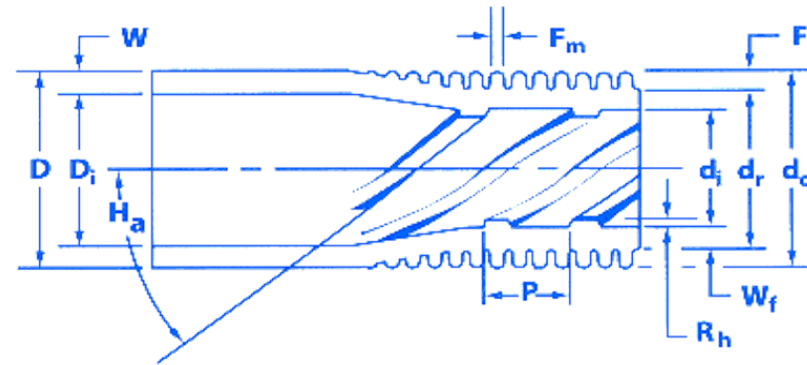


Spiral Grooved / Micro-fin



Indented / Corrugated

Internal Rib Geometry



Micro-fin ID: 3 Main Parameters:

No. Rib starts: 10 – 50

Rib Height: .010 - .016

Helix Angle: 20 – 45 degrees

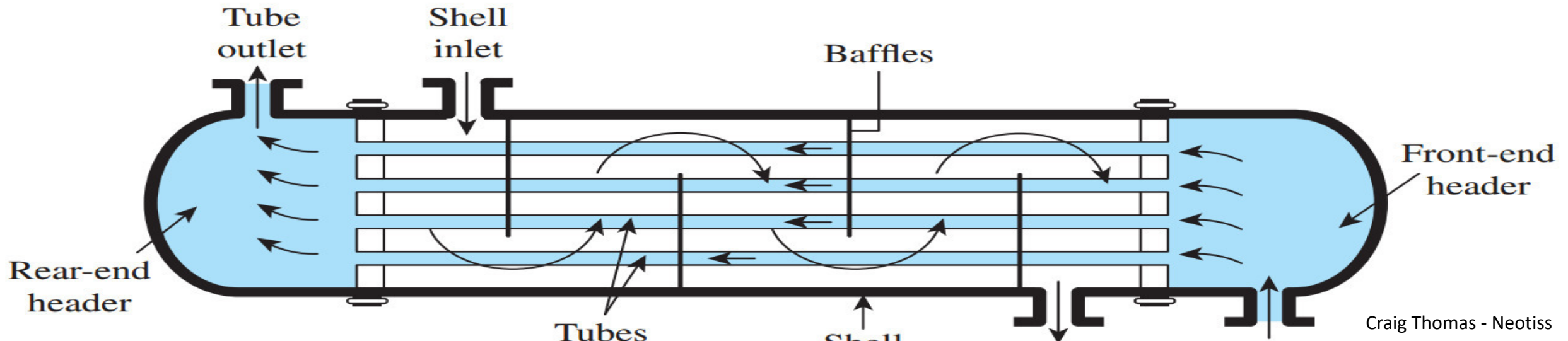
When to Consider ?

Tube-side controlling heat transfer

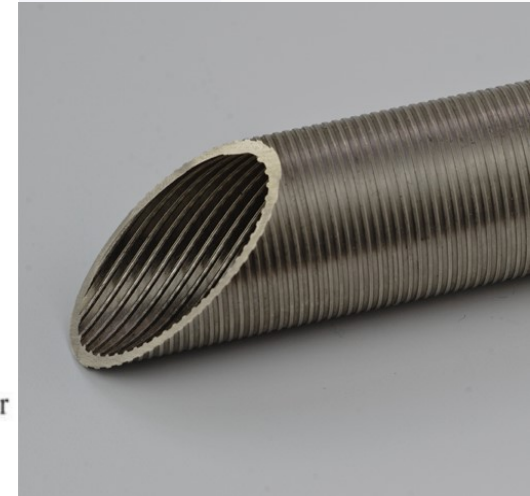
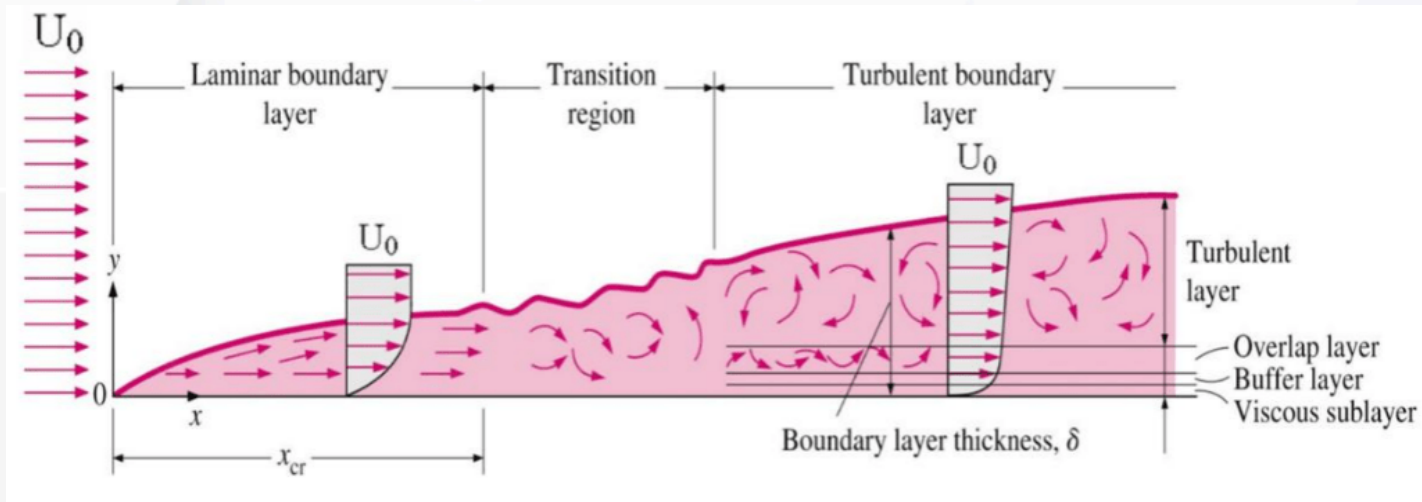
Space / weight restricted

Unused tube-side pressure drop

Debottlenecking / Retrofit

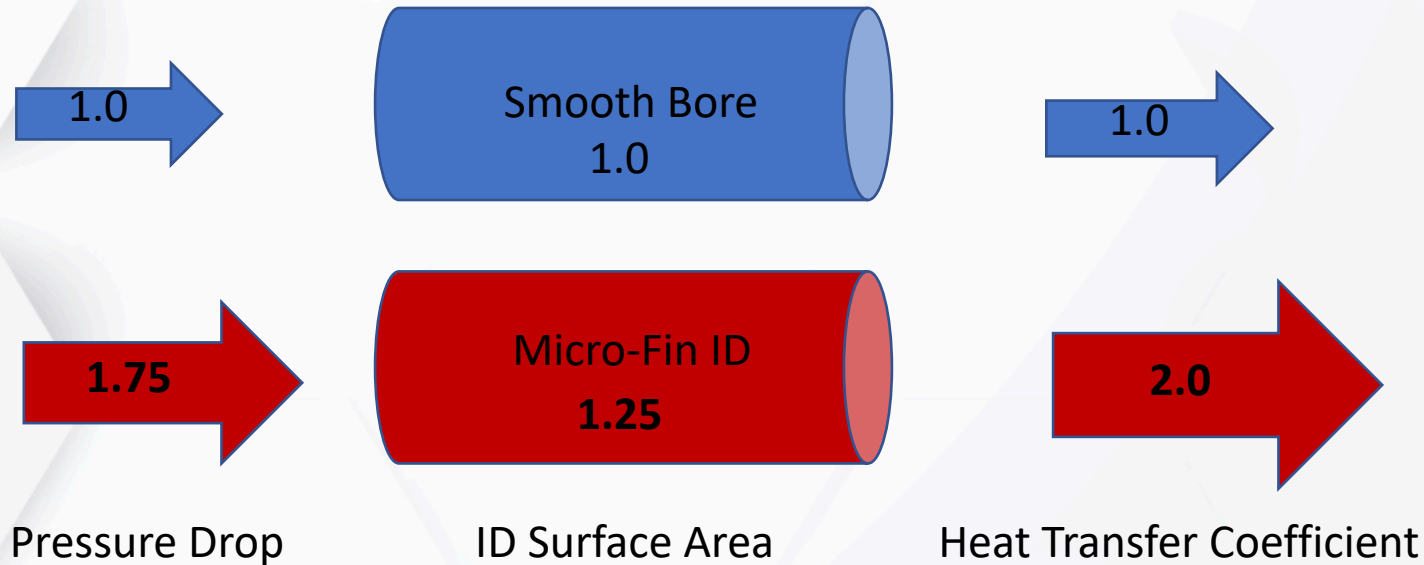


The Fluid Dynamics of Micro-fin ID Surface



Spiral grooves disrupt boundary layer
Increased shear stress at tube wall

Performance Comparison in Cooling Water



Sponsored by:



Predicting Performance

Typical Screening Design Multipliers

Service / Test Case	ID Heat Transfer	ID Pressure Drop	ID Area
Smooth bore reference standard	1	1	1
Single Phase (Cooling Water)	2.0	1.7	1.25
Two phase Condensing (N-Pentane)	1.5 to 2.3	1.4 to 1.8	1.25
Two Phase condensing mixture (n-Pentane / Paraxylene)	1.7 to 2.5	1.4 to 1.8	1.25



Industry Experience with Micro-fin ID tubing

Commercial Chiller Machine

- Refrigerant Evaporator
- Refrigerant Condenser



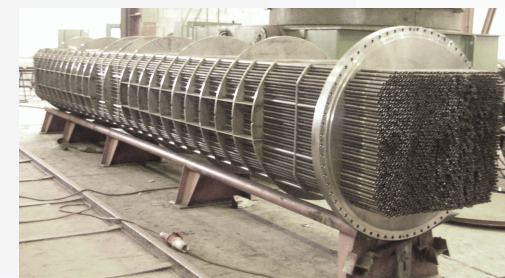
LNG Liquefaction Process

- C4/MR Evaporator
- C4 Condenser



Chem & Petrochem Pro

- Methanol Vaporizer
- C2 Splitter
- Recuperator

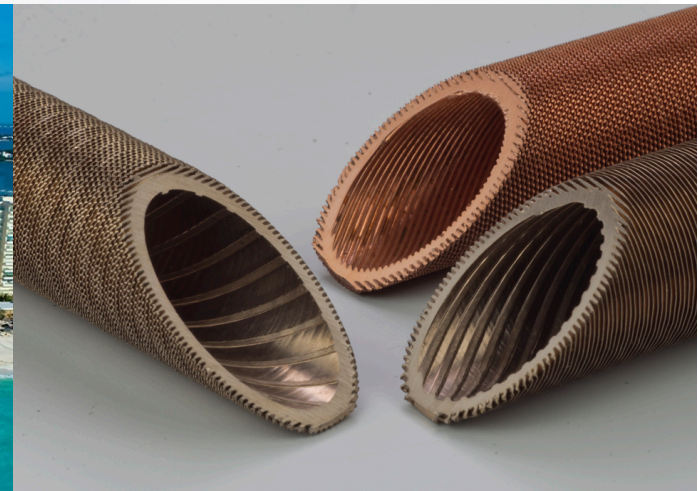


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Commercial Water Chiller Experience Micro-fin ID tubing

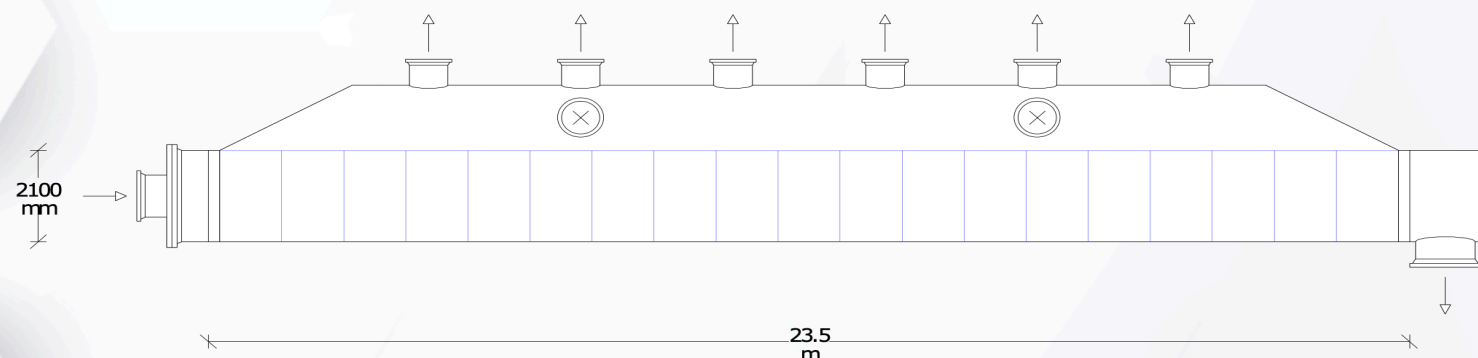
- 25+ Years of installation experience in all types of cooling water
- Over 200,000 Installations with cooling tower water since 1990
- **Over 200 installations with sea, river, brackish waters since 1999**
- 90% of all installations today use both OD and ID enhanced tubing



LNG Case Study

Precooling Section APCI Process

Propane Evaporating Shell-side / Mixed Refrigerant condensing Tube-side

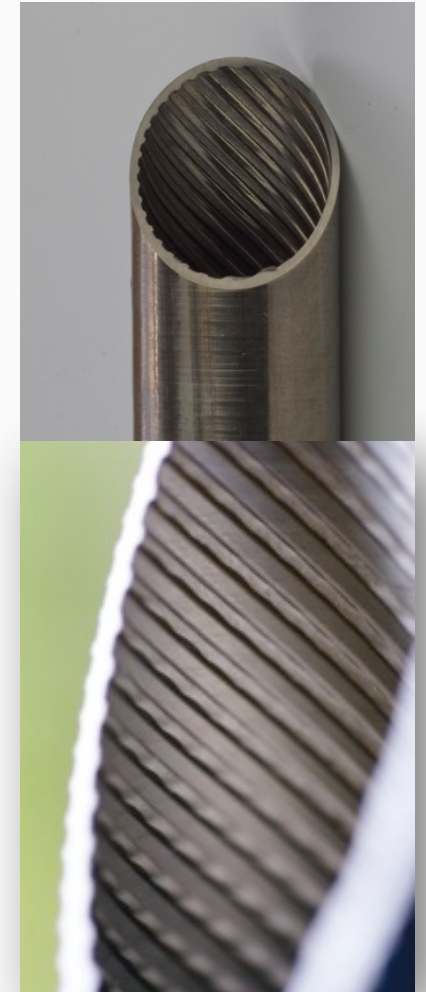
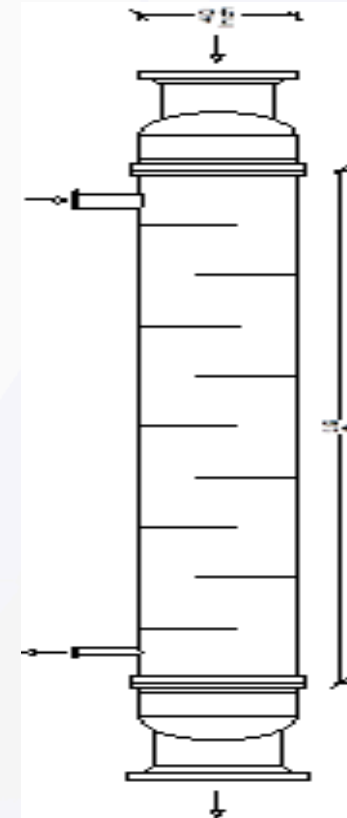


TEMA type	NKN	Total tube inlet nozzles	1	Stream ID	Shellside	Tubeside
Shell diameter	2100 mm	Total tube outlet nozzles	1	Stream name	Propane	Mixed Refrigerant
Kettle diameter	3599.99 mm	Total shell inlet nozzles	2	Flow, kg/s	98.7330	411.849
Tube length	23.5 m	Total shell outlet nozzles	6	Pressure drop, kPa	0.311	14.956
Dry weight	206081 kg/shell			Temperature, C	-34.02	-34.06
Wet weight	430205 kg/shell			Wt. fraction vapor	0.10000	1.00000
Bundle weight	127515 kg/shell			Pressure, kPa	143.198	142.888
						5750.00
						5735.04

Tube Type	Plain	OD Fin / Smooth Bore	Dual Enhanced
Tube Length Required (to meet Duty)	23.5M	16M	12.5M

Case Study: Methanol Vaporizer

Application: (Spray)	SS Steam / TS gas + Methanol liquid Vertical down flow
Problem:	Corrosion of CS tubes Not achieving 100% vaporization
Solution:	Replace CS with SS Tubes Use ID Enhanced Tubes
Results:	No issues after 10 years service. Same practice repeated in all their plants



Fouling and Spiral Grooved ID Tubing Research

Main principle: Higher shear stress at tube wall can lower fouling rate compared to smooth surface (however this is dependent upon many variables including fouling type, fluid velocity, and surface geometry)

R. Webb: In cooling tower water the lower the rib density (wider rib spacing)= lower fouling rate.

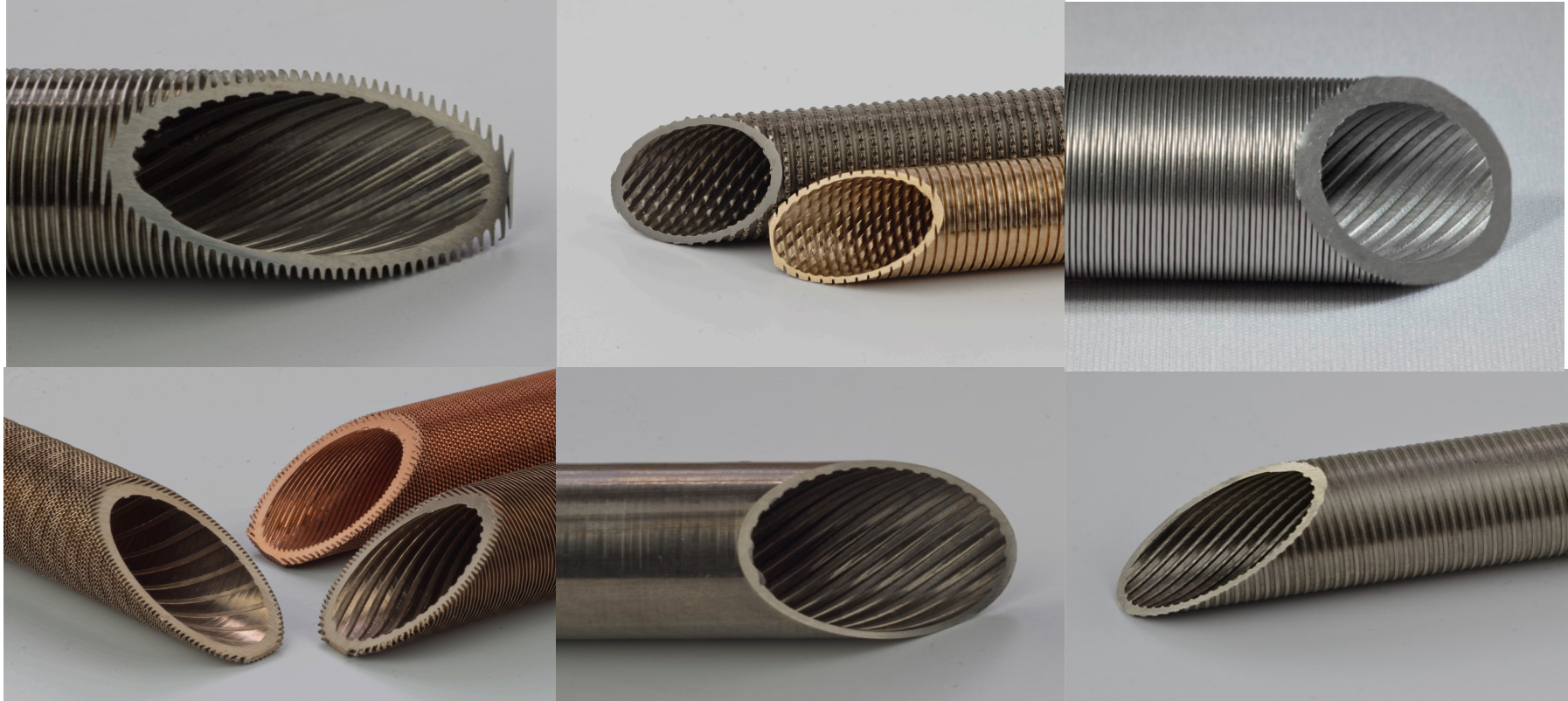
P. Thor: In cooling tower water the ratio of rib pitch / rib height of 3.5 is optimal to reduce fouling

H. Joshi: In crude oil the ID ribbed tube reduced fouling by 57% with HTFR + 21% and PD + 63%

C.B. Panchal: In seawater the shear stress in spiral fluted tubes can lift oxidized film from wall to prevent deposition.

ASHRAE Summary: Most significant variable in fouling rate is water quality not surface geometry. Next variable is water velocity. Then surface enhancement type. In cases where internal enhanced tubes do foul, they tend to maintain their performance advantage over smooth surface. Spiral grooved tubes can be cleaned with similar methods to smooth tubes.

Thank You!



Craig Thomas
NEOTISS, Inc.